



**COAL GASIFICATION PLANT FOR GENERATING
SYNTHETIC NATURAL GAS (SNG) AT BARDHAMAN,
WEST BENGAL (INDIA)**

COAL GAS INDIA LIMITED (CGIL)



Date 16.09.2026

CORRIGENDUM-I

NIT NO., : PNMM/PC-217/E/001 DATED 07.09.2026

**SUB. :COAL GASIFICATION PLANT FOR GENERATING SYNTHETIC NATURAL GAS
(SNG) AT BARDHAMAN, WEST BENGAL (INDIA)**

This is for information to all Bidders who are willing to participate in the subject NIT, that CORRIGENDUM-I date 16.09.2026 is being issued and shall be read in conjunction to the NIT and subsequent Amendments issued till date.

*All other terms & conditions of NIT shall be as per original NIT and subsequent Amendment(s).

For & on behalf of
COAL GAS INDIA LIMITED (CGIL)

Ritu Agarwal
16/09/26

(Ms. Ritu Agarwal)
Dy. General Manager & HOD (M.M)
Ph.:+ 91-9717104054
Email: rituagarwal@pdilin.com



**COAL GASIFICATION PLANT FOR GENERATING SYNTHETIC NATURAL GAS (SNG) AT
BARDHAMAN, WEST BENGAL (INDIA)
(NIT NO : PNMM/PC-217/E/001 Dated 07.09.2026)
Corrigendum I : Technical (Process) dated 16.09.2026**



SL. NO.	REFERENCE OF BIDDING DOCUMENT				AMENDMENT TYPE M/D/A	MODIFICATION
	Part/Sec.	Page No.	Clause No.	Description as per NIT		
1.	SEC-4.0	4 of 19	2.2.7 (Gasifier Configuration)	The technical proposal from the bidders shall be based on following two design cases: 1. Plant Design case (PDC case) 2. Equipment Design Case (EDC case) EDC design case has been specified with 18.4% overdesign margin on PDC case. Gasification Plant shall be designed for EDC case.....	M	The technical proposal from the bidders shall be based on following two design cases: 1. Plant Design case (PDC case) 2. Equipment Design Case (EDC case) EDC design case has been specified with 18.4 20% overdesign margin on PDC case. Gasification Plant shall be designed for EDC case.....
2.	Sec 5.1 (DESIGN PHILOSOPHY – PROCESS)	--	Sec 5.1	Sec 5.1 DESIGN PHILOSOPHY – PROCESS	A	<u>Sec. 5.1 “DESIGN PHILOSOPHY – PROCESS” of NIT, Part-II (Technical) is missing, same is being attached and shall form part of the Tender document.</u>

LEGEND:

M: MODIFICATION, A: ADDITION, D: DELETION.

Encls.: Sec 5.1 ‘DESIGN PHILOSOPHY – PROCESS’

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PART II: TECHNICAL

SECTION – 4.1

BATTERY LIMIT INTERFACE

PLANT: COAL GASIFICATION PLANT FOR GENERATING SYNTHETIC NATURAL GAS

PROJECT: SYNTHETIC NATURAL GAS PRODUCTION THROUGH COAL GASIFICATION ROUTE AT BARDAHMAN, WEST BENGAL (INDIA).

0	19/08/2026	16/09/2025	Issued for Tender Purpose	SK	TNN	MN
REV	REV DATE	EFF DATE	PURPOSE	PREPD	REVWD	APPD

	<u>COAL GASIFICATION PLANT FOR PROPOSED COAL TO SYNTHETIC NATURAL GAS</u> <u>OWNER: COAL GAS INDIA LIMITED</u> <u>BATTERY LIMIT INTERFACE</u>	PC217/E/4001/P-II/ SEC-4.1	0	
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SL. NO.	DESCRIPTION	SHEET NUMBER
1.0	Battery Limit Interface	3
2.0	Battery Limit Conditions	3

LIST OF ATTACHMENTS

SL. NO.	DESCRIPTION	NUMBER OF SHEETS
1.0		

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1.0 BATTERY LIMIT INTERFACE:

1.1 Interface Engineering:

LSTK Contractor shall carry out all interface engineering for complete compatibility with PDIL/ Coal Gas India Limited design with respect to location/ specification for all incoming and outgoing pipelines from Coal Gasification Plant.

1.2 Battery Limit Isolation:

LSTK Contractor shall provide double block and bleed arrangement with spectacle blind for all process and steam streams coming into and going out of the Coal Gasification Plant. For other utilities, LSTK Contractor shall provide isolation valves within their plant battery limit.

1.3 Metering System:

LSTK Contractor shall provide metering system for all incoming and outgoing process and utility streams as indicated in the instrument specification of the ITB.

2.0 BATTERY LIMIT CONDITIONS:

2.1 Feedstock supplied to **Coal Gasification Plant** shall be as follows:

Coal Analysis: - Refer, Annexure-I of Section- 4.0 Part-II Technical, for ECL coal (representative analysis considered to be confirmed by LSTK Contractor)

Fluxant: - (purity >95%).

2.2 Purified Syn. Gas :

Temperature and pressure condition of Purified Syn. Gas required at Coal Gasification plant battery limit shall be as follows:

Stream / Condition	Min	Normal	Max	Mech. Design
Purified Syn. Gas				
Header pressure, (kg/cm ² g)		30	-	By LSTK
Supply temperature, (deg C)	-	-	45	As per Design guidelines 5.1

2.3 Carbon Di-oxide:

Excess Carbon Dioxide shall be vented at suitable height .

2.4 Utility Nitrogen Gas:

Temperature and pressure condition of Nitrogen at Coal Gasification plant battery limit shall be as follows:

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LP Nitrogen	
Pressure, kg/cm²g (Min/Nor/Max)	6.0/8.0/9.0
Temperature	Ambient
N₂, Vol %, min	99.99%
O₂, Vol ppm	< 10
HP Nitrogen	
Pressure, kg/cm²g (Min/Nor/Max)	--/82/--
Temperature	80
N₂, Vol %, min	99.99%
O₂, Vol ppm	< 10

2.5 Sulphur (Liquid):

Temperature and pressure condition of Sulphur required at LSTK-1 plant Battery limit shall be provided as follows:

Stream / Condition	Min	Normal	Max	Mech. Design
Sulphur (Liquid)				
Supply pressure, (kg/cm ² abs)		5.5*	6.9*	8.4/FV*
Supply temperature, (deg C)		155*	165*	180*

Note: - * - figures are indicative. However Licensor's specifications to be followed.

FV = Full Vacuum

2.6 Flare: LSTK Contractor shall have to consider flaring requirement and piping up to LSTK B/L of Coal Gasification Plant.

Condition		Mech. Design
Pressure (sour gas)	*	*
Pressure (sweet gas)	*	*

* To be specified by LSTK Contractor

2.7 Cooling water shall be supplied by Owner for use in Coal Gasification Plant mperature and pressure condition of Nitrogen at Coal Gasification plant battery limit shall be as follows:

Condition	Min	Normal	Max	Mech. Design
Supply pressure, kg/cm ² g	-	4.5	-	10

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Return pressure, kg/cm ² g	-	3.0	-	10
Supply temperature, °C	-	33	-	70
Return temperature, °C	-	43	-	70

* To be specified by LSTK Contractor

Note: LSTK Contractor shall limit pressure drop of 1.5 Kg/cm² (max) between supply and return CW header within its battery limit.

2.8 De-Mineralised Water: make-up DM water shall be provided from balance of plants by OWNER to LSTK Contractor.

Condition	Min	Normal	Max	Mech. Design
Supply pressure, kg/cm ² g	4.0	5.5	6.0	10.0
Supply temperature, °C	-	Ambient		65

2.9 Service Water: to be provided by the Owner to the LSTK Contractor

Condition	Min	Normal	Max	Mech. Design
Supply pressure, (kg/cm ² g)	4.0	6.0	8.0	10.5
Supply temperature (deg C)	Ambient	Ambient	Ambient	65

2.10 Drinking water: to be provided by the Owner to the LSTK Contractor

Condition	Min	Normal	Max	Mech. Design
Supply pressure, kg/cm ² g		6.0	6.5	12.5
Supply temperature, (deg C)		Ambient	Ambient	65

2.11 Instrument Air: to be provided by the Owner to the LSTK Contractor

Condition	Min	Normal	Max	Mech. Design
Header pressure (kg/cm ² g)	6.0	8.0	10.0	10.5
Supply temperature (deg C)	Ambient	Ambient	50	65

2.12 Plant air: to be provided by the Owner to the LSTK Contractor

Condition	Min	Normal	Max	Mech. Design
Header pressure (kg/cm ² g)	4.0	7.0	8.0	10.5
Supply temperature (deg C)	40	40	50	65

2.13 Steam:

Steam	Pressure (kg/cm ² g)	Temperature (deg C)
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Level	Normal	Max	Min	Design	Normal	Max	Min	Design
HP	107	110	105	130	515	520	510	545
MP	40	*	*	44	380 ± 5	*	*	425
LP	4.0	4.5	3.5	6.0	180	*	*	250
HP Saturated)	107	110	105	130	315	317	314	342

* To be specified by LSTK Contractor

2.14 Electric Power: to be provided by the Owner to the LSTK Contractor

Power Supply	Voltage	Phase	Frequency
Normal Power (2 Nos.)	33000 V ± 10%	3	50 Hz ± 5%
Emergency Power (1 No.)	11000 V ± 10%	3	50 Hz ± 5%

2.15 Treated Condensate export from Coal Gasification Plant BL (applicable for Gas purification unit):

Description	Pressure (kg/cm ² g)				Temperature (deg C)			
	Min	Max	Normal	Design	Min	Max	Normal	Design
Treated Condensate			8	12			45	65

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2.16 Liquid Effluent from Coal Gasification Plant BL applicable for Gas purification unit:

Description	Pressure (kg/cm ² g)				Temperature (deg C)			
	Min	Max	Normal	Design	Min	Max	Normal	Design
Liquid Effluent			3	8			Amb.	65

Note: Coal Gasification Complex shall be designed based on Zero Liquid Discharge philosophy.